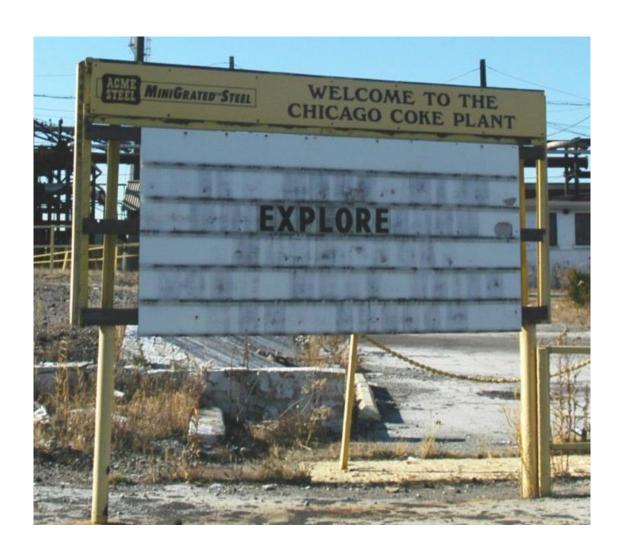
Acme Coke 11236 S. Torrence Ave. Chicago IL 60617



acmecoke.com

Document archive

Upgraded Ammonia Removal System Dated: 1994

ACME STEEL COMPANY

CAPITAL EXPENDITURE AUTHORIZATION SUMMARY

FINAL CEA

C.E.A. NO.

CI-4039-000-7

TEMP. NO.

PLANT Iron and Coke Operat	tions - Chic	ago C-2	981	ITEM NO CAPITAL PLAN:
PROJECT TITLE		450 0 2	.501	TOTAL CAPITAL AMOUNT IN CAPITAL PLAN:
Upgrade Ammonia Remo	oval			PROFIT PLAN: AQ QZQ GGG
COMPLETION TIME	PROFIT PLAN: \$2,270,000 REVIEW:			
(MONTHS FROM APPROVAL)	10	R.	Martello	ACTION .
CAPITAL FUNDS TO BE APPROV	VED:		DESCRIPTION AND	USTIFICATION:
Land	\$			
Buildings	_			vides for the upgrade of the sys
Equipment	2,173	,600		ammonia from the coke oven
Less: Cash value of				ne Chicago Coke Plant. Th
facilities replaced	\$			e required because of the fact to n of benzene emission contr
	0 170			of benzene emission control of resulted in the removal of
	\$,600	= Marley cooling	
			provided for	
				t will be necessary to install
TOTAL INVESTMENT:	\$_2,173	600		ompensate for the loss of t
Capital Funds	\$ 2,175	,000	facility.	ompensato 101 the 1000 of
Working capital				
Total	\$ 2,173	600	The Type II Pre	iminary project estimated the
				roject at \$1,550,000 (\$1,411,
				,000 expense). As a result of
JUSTIFICATION:				nal engineering, the scope the w
Discounted			has been revised	with various installations be
Cash Flow Return			w upgraded and exp	anded necessitating the use of m
				als and higher labor costs.
Payback Period				cost has now been finalized
				173,600 capital and \$140,
			expense).	
RELATED EXPENSES:				
Expense:				es in the need to provide effect
Project	\$140,	000		in order to prevent accelera
Start-up				ne plant's coke oven gas pip
	110		systems.	
Total	\$140,	000	_	
			1	
A RICHIER SEE			APPROVED BY	
TITLE			SIGNATURE	DATE
1. Vice President - (nerations	1		
Arce Hestdellt - (peractons			
2. President				

5.

6.

Treasurer

President and COO/AMI

Chairman and CEO/AMI

Board of Directors

PROJECT NO.

DESCRIPTION OF PROJECT						
PROJECT TITLE						
Upgrade Ammonia Removal	DESCRIPTION OF PROJECT PLANT Iron and Coke Operations - Chicago					
DEPARTMENT OR COST CENTER						
C-2981	Iron and Coke Operations - Chicago					

This project provides for the upgrade of the system used to remove ammonia from the coke oven gas produced at the Chicago Coke Plant. Completion of these upgrades is required to provide effective ammonia removal to prevent accelerated corrosion in the plant's coke oven gas piping system.

As detailed in Schedule "B", the amount approved originally was \$1,550,000 consisting of capital funds of \$1,411,000 and expense monies of \$139,000. The revised estimated total cost is \$2,313,600 of which \$2,173,600 is capital and \$140,000 is expense. Hence, the final cost will exceed the preliminary estimate by a total of \$727,100 including additional capital funds of \$726,100 and \$1,000 expense.

The following discussions by sub-account detail the major reasons for the overruns:

Sub-Account No. 100: Purchase New Tanks (Capital)

Approved: \$205,000 Additional Authorization Requested: \$25,000 Total: \$230,000

The primary reason for this overrun is price escalation for the new tanks of \$18,200 due to increases in the cost of stainless steel. Additionally, in order to expedite the delivery of the new tanks by six weeks, the second low bidder was awarded the purchase order at a higher cost of \$4,000.

Sub-Account No. 300: Purchase Equipment (Capital)

Approved: \$229,000 Additional Authorization Requested: \$35,800 Total: \$264,800

Additional authorization is required for the purchase of equipment that was omitted from the original estimate. These items include motor starters (\$18,000), a loading bridge and arm (\$7,700), a control panel (\$6,100), and a blower (\$2,200).

Sub-Account No. 400: Install Foundations and Structures (Capital)

Approved: \$134,800 Additional Authorization Requested: \$216,200 Total: \$351,000

The original cost was based on preliminary Acme Engineering estimates that were formulated before any detailed design work was accomplished. As such, all estimates were based on simple schematic flow charts that summarized the philosophy of the processes without actually defining precise physical locations, distances and elevations. The original estimate for concrete work assumed the installation of 171 cubic yards of concrete. As a result of final engineering, it has been determined that these foundations were inadequate. The revised foundations require 257 cubic yards of concrete requiring additional funds of \$97,700. Additionally, as a means of protecting concrete slabs in the tank areas from attack by corrosive acids and ammonium sulphate solutions, a decision was made to protect the concrete surfacing with a reinforced epoxy overlay at a cost of \$67,500. Furthermore, the final cost to install two pumphouse buildings will exceed the original estimate by \$31,300 while the cost of structural steelwork will require additional funds totalling \$16,500.

DESCRIPTION	OF	PRO.	JECT
-------------	----	------	------

PROJECT NO.		18

PROJECT TITLE

Upgrade Ammonia Removal

PLANT

C-298

Iron and Coke Operations - Chicago

Sub-Account No. 500: Mechanical Installation (Capital)

Approved: \$239,000 Additional Authorization Requested: \$366,400 Total: \$605,400

The original cost estimate for mechanical installation included a provision for material of \$89,000. The cost of materials has now been finalized at \$265,400 resulting in an overrun of \$176,400. The primary reason for this increase is that the original estimate assumed the use of electric resistance welded pipe whereas the final costs are based on the installation of more expensive seamless pipe along with seamless fittings and "Alloy 20" check valves. The use of these upgraded materials was deemed necessary because observations of recent installations of welded pipe and fittings indicated that they would be unable to provide an acceptable service life due to inability of the welds to withstand deterioration from corrosive fluids. An aditional contributing factor for the overrun in material costs is escalation resulting from price increases for stainless steel.

The original estimate for mechanical installation included a labor cost provision of \$130,000. The revised estimate of \$254,700 resulted in an overrun of \$124,700. The primary reason for the additional costs is that during final engineering, it was determined that a significant amount of new piping is being installed within the Sulphate Building. Since this facility has been determined to be a hazardous area where welding is not permitted, the labor cost was understated. The revised scope requires the contractor to obtain detailed field measurements of facilitites within the Sulphate Building and to subsequently complete welding work onsite outside of the building or within a local shop resulting in extreme inefficiences.

An additional factor contributing to the labor cost overrun is that extra costs are required to complete specialized welding procedures required for stainless steel. Also, as mentioned earlier, the entire cost estimate was based on preliminary flow diagrams lacking necessary specification and details.

The cost of the final scope of work has also increased by a total of \$69,300 due to installation of new equipment that was deemed necessary as final engineering progressed. Major additions include \$44,500 for steam and condensate piping to prevent certain pipelines from freezing, \$12,600 for the venting of tanks within the Sulphate Building for safety reasons, and \$12,200 for city water connections associated with the installation of five eyewash and safety shower stations.

Sub-Account No. 700: Electrical Installation (Capital)

Approved: \$180,000 Additional Authorization Requested: \$108,900 Total: \$288,400

The amount originally requested was based on a 1991 Acme Engineering estimate that was formulated by comparing the preliminary scope of work with the actual electrical costs incurred for the completion of the Benzene NESHAP Capital Project (CI-3005). Once again, the preliminary scope was formulated before any engineering design work had been accomplished. The comparison involved an estimate of the number and size of motors and controls as compared to a listing of actual costs incurred for electrical installations for the Benzene NESHAP project. From this comparison, an order-of-magnitude factor was used to estimate the electrical costs required for the ammonia removal project. The amount being requested in this Final CEA is now based on a competitive quotation.

DES	CRIPT	HON	OF	PRO	JECT

PROJECT NO.	

	DESCRIPTION OF PROJECT
PROJECT TITLE	
Upgrade Ammonia Removal	PLANT
DEPARTMENT OR COST CENTER	Iron and Coke Operations - Chicago
C-2981	Tron and coke operations that

Sub-Account No. 950: Contract Engineering (Capital)

Approved: \$114,000 Additional Authorization Requested: \$33,000 Total: \$147,000

The original estimate was an average of competitive quotes based on the preliminary scope of work plus an allowance of 5% for scope increases. Additional authorization of \$15,500 is now required for greater than anticipated scope additions plus \$17,500 for additional services performed including soil testing (\$8,500), procurement of permits (\$6,000), and completion of a land survey (\$3,000).

Although the ammonia removal system will not be physically complete for ten months, the system will be operational four months after the approval of this supplement.

Justification of this expenditure lies in the need to install an ammonia removal system in order to prevent accelerated corrosion in the plant's coke oven gas piping system.

CALCULATION OF EXPENDITURE REQUIRED
AND EXPENDITURE PAYOUT PERIOD

PLANT

PROJECT NO.

Iron and Coke Operations - Chicago

SUB-ACCOUNT	CHECK DIGIT	DESCR		ENDITURE AMO		7,0000111		
NUMBER	NUMBER *			CAPI	TAL EXI	PENSE	DISTRIBUTION	
		APPROVED	PREVIOUSLY APPROVED		ADDITIONAL AUTHORIZATION REQUESTED		TOTAL TO BE EXPENDED	
		CAPITAL	EXPENSE	CAPITAL	EXPENSE	CAPITAL	EXPENSE	
55 Site Prep	aration	\$	\$ 21,000	\$	\$ 1,000	\$	\$ 22,000	
065 Disposal		-	90,000				90,000	
.00 Tanks		205,000	-	25,000		230,000	-	
00 Equipment		229,000	-	35,800		264,800		
00 Install Fo		134,800	-	216,200	-	351,000(1)	
00 Mechanical	Installation	239,000	-	366,400		605,400(2)	
00 Electrical	Installation	180,000		108,900		288,900(3)	
00 Spares		23,000		-		23,000		
50 Taxes		36,600				36,600	1	
70 Freight		10,000		/		10,000	-	
20 Acme Engin	neering	25,200				25,200		
40 Field Engi	neering	67,200	-	-	-	67,200		
50 Contract E	ingineering	114,000		33,000		147,000		
60 Employee T Start-up A		-	20,000	-		_	20,000	
70 Contingenc	y - Capital	147,200	-	(22,700)		124,500	-	
80 Contingenc	y - Expense		8,000	<u> </u>			8,000	
		\$1,411,000	\$139,000	\$762,600	\$ 1,000 \$	\$2,173,600*	\$140,000	

- (1) Based on quotations from Fred Berglund & Sons, Inc. dated November 14, 1994, for \$213,645; American Lining Systems, Inc. dated December 7, 1994, for \$67,900; Phoenix Welding Company, Inc. dated November 21, 1994, for \$66,500; and Overdoors of Illinois, Inc. dated October 5, 1994, for \$3,118 for a total of \$351,165.
- (2) Based on a quotation from Borg Mechanical Contractors, Inc. dated November 2, 1994, for \$605,406.
- (3) Based on a quotation from Meany Electrical Engineering Co. dated December 2, 1994, for \$288,918.
- * Capital Sub-Account Distribution: C-0025-0900
 ** Expense Sub-Account Distribution: C-0025-0900

PROJECT TITLE

Upgrade Ammonia Removal

REPLACEMENT AND REHABILITATION

ACME STEEL COMPANY

CAPITAL EXPENDITURE AUTHORIZATION SUMMARY

CI-4039-000-

PLANT		TYPE II PREL	IMINARY *
Iron and Coke Opera	tions - Chicago	C-2981	ITEM NO CAPITAL PLAN:
Upgrade Ammonia Remo	oval		TOTAL CAPITAL AMOUNT IN CAPITAL PLAN:
COMPLETION TIME	OVAL	PROJECT SPONSOR	PROFIT PLAN: #4 \$1,200,000
(MONTHS FROM APPROVAL)	6	A. Schwaighart	REVIEW:
CAPITAL FUNDS TO BE APPRO	VED:	DESCRIPTION AND	JUSTIFICATION
Land	\$		ovides for the upgrade of the syst
Buildings			ammonia from the coke oven
Equipment	1,411,000		the Chicago Coke Plant. The
Less: Cash value of			re required because of the fact th
facilities replaced	2		on of benzene emission contro
	\$ 1,411,000	Marley cooling	991 resulted in the removal of tower. Since this tower h
		provided for	some ammonia removal throu
			it will be necessary to install n
TOTAL INVESTMENT:	1 /11 000		compensate for the loss of th
Capital Funds	\$_1,411,000	facility.	
Working capital	Table 1 - Control of the Control of	The proposed	system will consist of
Total	\$ 1,411,000		processing arrangement. With t
			, three interchangeable new tan
			zed to perform the functions
JUSTIFICATION:	1		lution to the ammonia absorbe
Discounted		fresh acid solu	ne ammonia solution, and stori
Cash Flow Return		70	ution. Subsequently, the solution two new sulphate storage tanks.
Payback Period			
		Justification II	es in the need to provide effecti in order to prevent accelerat
		corrosion in t	the plant's coke oven gas pipi
RELATED EXPENSES:		systems.	me plane s coke oven gas pipi
Expense:	100 000		NINARY ECCTIVACE OF THE COOK OF THE
Project	\$ 139,000		MINARY ESTIMATE OF THE COST OF TH VAL IS BEING REQUESTED AT THIS TI
Start-up	-	TO SPEND \$609.8	00 FOR THE PURCHASE OF LONG LE
	\$ 139,000	ITEMS AND FOR	FINAL ENGINEERING. A FINAL C
Total		REQUESTING APPR	OVAL TO SPEND THE ENTIRE AMOUNT
		(TOTAL PRELIMINA	RY ESTIMATE \$1,411,000) BASED ON
		FINAL ESTIMATE (F THE TOTAL COST WILL BE SUBMITTE
		AT A LATER DATE.	
TITLE		APPROVED BY SIGNATURE	
1. President and COO		1 . 1	DATE
. Ilesident and coo		S.A. Sennett	3-27-94
2. Treasurer		Xelliam	3/28/94
3. Chairman and CEO		mman	3/2/94
Acme Steel Company 4. Board of Directors	Forh a	2.10 - 4 . 0	0 80 1 -1 -1-1
Acme Metals Incorp	orated /	of selectors to	+ Ale 3/28/94
5. Board of Directors	701 che ason	and of Deceter, 6	1 Glab 4/28/94
6.		1	sal. ARC.
M-5922-2			

	FRACE INC.
DESC	RIPTION OF PROJECT
PROJECT TITLE	
Upgrade Ammonia Removal	
DEPARTMENT OR COST CENTER	PLANT
C-2981: Cyanide & Ammonia Control	Iron and Coke Operations - Chicago

This project provides for the upgrade of the system used to remove ammonia from the coke oven gas produced at the Chicago Coke Plant. These modifications are required because of the fact that the recent installation of benzene emission controls (CI-9083) resulted in the removal of the Marley cooling tower. Since this tower had provided for some ammonia removal through air-stripping, it will be necessary to install new equipment to compensate for the loss of this facility in order to prevent accelerated corrosion of the plant's coke oven gas piping.

At present, the removal of ammonia from the coke oven gas is primarily accomplished as a batch process at the ammonium sulphate plant which is located before the final cooler in the by-product train. The process entails the spraying of the gas with a solution of sulphuric acid and water at the ammonia absorber to remove the entrained ammonia. The acid and water solution is subsequently recycled until it is saturated with ammonium sulphate. When the proper concentration is reached, the entire batch of sulphate solution, which totals approximately 10,000 gallons, is neutralized to meet specifications and sold as an aqueous product referred to as "SUL-900". The total batch processing time is approximately 26 hours of which six hours is the time required to neutralize the product. During the neutralization process, the flow of acid to the batch is shut off. Accordingly, as the quantity of free acid within the circulation system is diminished, the amount of ammonia that remains in the gas stream increases. With the previously existing final cooler system, the potential existed to strip some of this remaining ammonia from the gas at the final cooler system's Marley cooling tower.

As part of the benzene emission control system that was recently installed to comply with Federal NESHAP standards, the existing open Marley cooling tower was replaced with an enclosed wet surface air cooler. This cooler uses non-contact mill water and forced air to cool the tar/water media. This enclosed facility does not, however, provide for any ammonia removal.

This project provides for the installation of equipment to enhance the plant's ammonia removal potential by converting the existing batch processing configuration to a multiple batch processing arrangement. With the proposed system, three interchangeable new tanks will be utilized to perform the functions of circulating solution to the ammonia absorber, neutralizing the ammonia solution, and storing fresh acid solution. The system will consist of three 12,000 gallon tanks with necessary piping, process pumps and instrumentation. The neutralization process will be accomplished with an aqua ammonia solution. The proposed process design will allow the concentration of free acid in the absorber circulation system to be continuously maintained at a level of 4%. This increase should return the ammonia removal efficiency to the original design standard of 6 to 10 grains ammonia per 100 standard cubic foot of coke oven gas and significantly reduce corrosion rates. The acid flow rate will be regulated automatically by an automatic titration unit.

From the proposed neutralization sytem, the solution will be pumped to two new ammonium sulphate storage tanks. The tanks will be equipped with load in/load out nozzles, electric heaters capable of maintaining a solution temperature of 70 degrees Fahrenheit, and internal air agitation. The tanks will be constructed of fiberglass reinforced plastic to protect them from the corrosive effects of the ammonium sulphate. In total, the two tanks will be capable of storing 40,000 gallons of ammonium sulphate.

	Prodect No.
DESCRIPTION	OF PROJECT
Upgrade Ammonia Removal	
DEPARTMENT OR COST CENTER	PLANT
C-2981: Cyanide & Ammonia Control	Iron and Coke Operations - Chicago

TREO IECT NO

This Type II Preliminary project provides for final engineering and for the purchase of long-delivery equipment. Specific items that will be purchased include three circulation tanks, two ammonium sulfate storage tanks, one aqua ammonia storge tank, pumps, and electronic controls and instrumentation.

Justification of this expenditure lies in the need to install an ammonia removal system in order to prevent accelerated corrosion in the plant's coke oven gas piping system.

CALCULATION OF EXPENDITURE REQUIRED
AND EXPENDITURE PAYOUT PERIOD

PROJECT NO.

PROJECT TITLE		AND EXPENDITUR		PLANT	
Upgrade Ammo	onia Removal				erations - Chicago
SUB-ACCOUNT NUMBER	CHECK DIGIT NUMBER *	DESCRIPTION		EXPENDITURE AMOUNT CAPITAL EXPEN	IT ACCOUNT
		TYPE II AMOUNT TO B AUTHORIZED	E	TOTAL PROJ	ECT
055 Site Pre		CAPITAL \$	EXPENSE \$9,000	CAPITAL \$ —	EXPENSE \$ 21,000
065 Disposal		-	-		90,000
100 Purchase	New Tanks	205,000(1)	- /**	205,000	
300 Purchase	Equipment	229,000(2)	-	229,000	-
400 Install Structur	Foundations & es	_	-	134,800	-
500 Mechanic	al Installation	_	-3	239,000	
700 Electric	al Installation		- 1	180,000	- 18 m
800 Spares		_	- 0	23,000	_
850 Taxes		36,600	-	36,600	_
870 Freight		_	_ 4	10,000	_
920 Acme Eng	ineering	25,200	- 3	25,200	
940 Acme Fie	ld Supervision	_	- 3	67,200	-
950 Contract	Engineering	114,000(3)	()	114,000	_
960 Employee Start-up	Training & Allowance		_	_	20,000
970 Continger	ncy - Capital	_	5	147,200	_
980 Continger	ncy - Expense	<u> </u>	(_		8,000
	TOTAL	\$609,800	\$9,000	\$1,411,000	\$139,000
	GRAND TOTAL	\$618.8	800	\$1,550,	000

⁽¹⁾ Based on a quotation from Kennedy Tank and Manufacturing Co., Inc. dated October 19, 1993, for \$150,359 (Andcor, Inc. provided a verbal quote of \$156,760. Imperial Steel Tank Company quoted \$167,750 on October 12, 1993. Creco, Inc. quoted \$183,028 on October 14, 1993. Chicago Boiler quoted \$198,130 on October 20, 1993. Standard Boiler & Tank Company quoted \$199,460 on October 15, 1993) plus a quotation from Creco, Inc. dated October 15, 1993, for \$54,502 (Plastic Piping Systems, Inc. quoted \$61,294 on October 14, 1993. Andcor, Inc. quoted \$63,096 on October 27, 1993. Viatec Hastings Engineered Systems quoted \$68,924 on October 19, 1993. Xerxes Corporation quoted \$94,615 on October 18, 1993) for a total of \$204,861.

CALCULATION OF EXPENDITURE REQUIRED

PROJECT NO.

1 18 4 1 1 1 1 1 1		AND EXPENDITURE PA			
PROJECT TITLE			PLANT		
Upgrade Ammonia Removal			Iron and Coke Operations - Chicago		
SUB-ACCOUNT NUMBER	CHECK DIGIT NUMBER *	DESCRIPTION	EXPENDITURE AMOUNT		ACCOUNT
			CAPITAL	EXPENSE	DISTRIBUTION

- (2) Per Acme engineering based on numerous quotations and engineering allowances.
- (3) Based on a quotation from Meca Engineering Corp dated September 7, 1993, for \$113,940. (R. T. Patterson Co, Inc. quoted \$116,800 on August 30, 1993. Orbital Engineering, Inc. quoted \$152,000 on August 31, 1993. Eichleay Engineers, Inc. quoted \$151,600 on September 7, 1993. ATSI, Inc. quoted \$258,100 on September 1, 1993.)

NOTE: All other estimates based on Acme Engineering project development.

EXPENDITURE PAYOUT PERIOD

COKE PLANT DECEMBER 8, 1994

TO:

JOE DIMAURO

FROM: JACK GARZELLA

SUBJECT: PUSHING EMISSIONS

WITH THE INSTALLATION AND COMMISSIONING OF THE ENHANCED AMMONIA REMOVAL PROCESS, THE CORROSION RATES SHOULD BE SIGNIFICANTLY REDUCED.

THE DISTRIBUTION SYSTEM, REVERSING COCKS, PIPING, HEADERS, ORIFICES, PINS, AND NIPPLES WILL NOT PLUG WITH DEPOSITS AS FREQUENTLY. THE RATE OF FOULING WILL BE REDUCED. HENCE, THE PUSHING EMISSION SHOULD IMPROVE.

CC: D. O'HEHW C.D. STAFF

INTEROFFICE CORRESPONDENCE

Copies to:

Date: November 28, 1994

S. D. Bennett R. J. Martello

To:

J. A. DiMauro

From:

J. Garzella, M. T. McCarthy, A. C. Schwaighart

Subject:

AMMONIA REMOVAL UPGRADE

CC!

Reference:

The following is a status report for the Ammonia Removal Upgrade, Project CI-4039.

1. Final Engineering

Contract Engineering by R. T. Patterson:

Mechanical:

100% complete 100% complete

Instrumentation:

Civil/Structural: Design Drawings complete except for minor

details

Electrical:

Design Drawings complete except for minor

details

2. Procurement

Requisitions for all equipment to be furnished by Acme have been processed except the control panel. This requisition will be processed by November 29. Placement of all purchase orders should be completed by December 2.

3. Installation

Mechanical:

Bid packages sent out November 2. Quotations

due November 21.

Structural:

Bid packages sent out November 2. Quotations were received and purchase orders placed for site preparation, excavation and foundations. Quotations for remaining work due November 21.

Electrical/ Instrumentation:

Specification was completed and sent out for

bid. Quotations will be due by November 28.

Schedule:

Schedule slippage from a January to mid-March completion resulted from longer than projected durations to complete final engineering and specification preparation. Efforts to improve the schedule will include acceleration of order placement for some items of work (e.g., site prep., excavations and foundations) and expedition of construction activities.

CI-4039 AMMONIA REMOVAL UPGRADE - CONSTRUCTION SCHEDULE (TENTATIVE)

CC:STMP
1309 INTEROFFICE CORRESPONDENCE January 23, 1995 J. A. DiMauro TO: cc: G. S. Lucenti FROM: J. Garzella R. J. Martello M. T. McCarthy SUBJECT: Upgrade Ammonia Removal - CI-4039 Attached are the status report and bar chart schedules for this project. The project completion schedule is based on approval of the Final CEA by late January. Completion of the installation is planned for mid-July, however, start-up of the upgraded system is planned for early May. J. Garzella

R. J. Martello Am

M. T. McCarthy work-

JG/RJM/MTM/jm

UPGRADE AMMONIA REMOVAL

PROJECT STATUS

1.00 ENGINEERING

- 1.01 A Final CEA project was written on 1/10/95 for the current estimated cost to complete the project.
- 1.02 Installation design engineering is 98% complete.
- 1.03 Work associated with obtaining a city of Chicago building permit is in progress.
- 1.04 The IEPA construction permit application was prepared and submitted.

2.00 PROCUREMENT

- 2.01 Tanks
 - o Fabrication is 70% complete.
 - o Deliveries are scheduled for 2/13/95 through 2/24/95.
- 2.02 Pumps and Mixers
 - o 100% Delivered
- 2.03 Instruments
 - o 90% Delivered
- 2.04 Control Panels
 - o Fabrication is 25% complete.
 - o Delivery is scheduled for 2/15/95.
- 2.05 Control Valves
 - o 100% Delivered
- 2.06 Motor Starters
 - o Purchase Order issued 1/17/95.
- 2.07 Miscellaneous Equipment
 - o 25% Delivered

2.08 Spares

o No work to date.

3.00 CONSTRUCTION/INSTALLATION

3.01 Foundations and Buildings

- o Purchase Order issued 11/18/94.
- o Storage tank farm and pump house foundations are 85% complete and are (5) days behind schedule due to severe cold weather during w/o 1/2/95.
- o Process area foundations work was started 1/19/95.
- o Masonry work is scheduled to start w/o 1/23/95.

3.02 Structural Steelwork

- o Purchase Order issued 12/16/94.
- o Shop detail drawings are 75% complete.
- o Fabrication is 25% complete.

3.03 Piping/Mechanical

- o Purchase Order issued 12/27/94.
- o Contractor material procurement is 90% complete.
- o Pipe spools fabrication started 1/3/95 and is 30% complete.

3.04 Electrical/Power & Control

- o Purchase Order issued 12/27/94.
- o Embedded grounding in the storage tank farm was completed 1/4/95.
- o Contractor material procurement is 90% complete.
- o Installation of conduit is scheduled to start 2/13/95.

4.00 TRAINING

4.01 Training Services

o A proposal to furnish training manuals and training sessions was received on 1/19/95 and is being reviewed.

Light Lots of table

July 1995 June 1995 - ISTART-UP------May 1995 April 1995 March 1995 February 1995 COMPLETION OF THE INSTALLATION IS PLANNED FOR MID-JULY HOURDLER, START-UP OF THE UPGRADED SYSTEM IS PLANNED FOR EARLY MAY. START-UP 05-01-95 to 05-29-95 [28 days] January 1995 FINAL CEA-December 1994 FINAL CEA 12-26-94 to 01-30-95 [35 days] 01/23/95 C14039 Upgrade Ayionia Remojal Installation Schedule Sumary ovember 1994 THIS SCHEDULE IS BASED ON APPROVAL OF THE FINAL CEAPROJECT BY LATE JANUARY. 5.0 START-UP & DEBUG 4.0 INSTRUMENTATION FINAL CEA PROJECT 1.0 STRUCTURAL 2.0 MECHANICAL 3.0 ELECTRICAL

June 1995 12 19 February 1995 6 13 20 T December 1994 January 1995 ber 1994 14 21 1.4.1 Install Access Portal 1.6 Control Room Modification 1.8 Inst! Protective Overlay 1.3.1 Install Foundations 1.4.2 Install Foundations 1.3.3 Install Steelwork 1.4.3 Install Steelwork 1.5.1 Repair Foundation 1.3.2 Install Masonry 1.5.2 Install Masonry 1.8.3 Acid Pump House 1.8.2 Sulphate Room 1.8.1 Storage Area 1.5 Acid Pump House 1.7 Grout Equipment 1.2 Site Prep (Demo) 1.4 Sulphate Room 1.3 Storage Area 1.1 Mobilize 1.0 STRUCTURAL

01/22/95 C14039 Upgade Aptonia reyolal Installation schedule Sheet I of 3

92 June 1995 12 19 April 1995 10 17 February 1995 T January 1995 9 16 23 December 1994 12 19 ber 1994 14 21 2.13 Install Pipe Insulation 2.6.2 Tanks 34025,27,428 2.6.3 Storage Area Pumps 2.6.4 Process Area Pumps 2.6.1 Tanks 34018,19421 2.9 Install Temp Acid Pump 2.16 Decon Exist Sul Tank 2.14 Relocate Circ Pumps 2.17 Demo Exist Sul Tank 2.8 Install Supports 2,10 Install Tracing 2.1 Procure Material 2.4 Fab Pipe Spools 2.15 Tie-in Piping 2.3 Mobilize Field 2.7 Install Piping 2.6.5 Acid Pumps 2.12 Flush Piping 2.6 Set Equipment 2.2 Mobilize Shop 2.5 Fab Supports 2.11 Test Piping 2.0 MECHANICAL

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June 1995 12 19 24 April 1995 10 17 March 1995 13 20 February 1995 1..... 92 December 1994 12 19 82ber 1994 14 21 3.3 Install Embedded Grdng 4.1 Calibrate & Commission 3.5 Install Mtr Starters 3.6 Install Control Pnis 3.11 Install Cond & Cable Acid Pump House 3.2 Procure Material 3.4 Install Conduit 3.8 Terminate Cable 3.7 Install Cable 3.9 Temp Acid Pump 3.10 Test Systems 5.0 START-UP & DEBUG 4.0 INSTRUMENTATION 3.1 Mobilize 3.0 ELECTRICAL

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